

**SIDDHARTH INSTITUTE OF ENGINEERING & TECHNOLOGY:: PUTTUR**  
(AUTONOMOUS)

**B.Tech II Year I Semester Regular & Supplementary Examinations December-2023**

**HEAT & MASS TRANSFER**

(Agricultural Engineering)

**Time: 3 Hours**

**Max. Marks: 60**

(Answer all Five Units 5 x 12 = 60 Marks)

**UNIT-I**

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|---|---|---|-----|----|----|
| 1 | a | List the basic laws which govern the heat transfer. | CO1 | L1 | 6M |
|   | b | Name and explain the mechanism of heat transfer.    | CO1 | L1 | 6M |

**OR**

- |   |   |   |     |    |    |
|---|---|---|-----|----|----|
| 2 | a | What is conduction heat transfer? Explain its parameters  | CO1 | L1 | 6M |
|   | b | A plane wall is 150 mm thick and its wall area is 4.5 m <sup>2</sup> . If its conductivity is 9.35 W/m °C and surface temperature are steady at 150 °C and 45 °C, determine i).Heat transfer across the plane wall, ii).Temperature gradient in the flow direction. | CO1 | L4 | 6M |

**UNIT-II**

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|---|---|---|-----|----|----|
| 3 | a | Derive an expression for heat conduction through a composite wall.  | CO2 | L3 | 6M |
|   | b | A reactor's wall, 320 mm thick, is made up of an inner layer of fire brick (k = 0.84W/m °C) covered with a layer of insulation (k = 0.16 W/m °C). The reactor operates at a temperature of 1325 °C and the ambient temperature is 25°C. Determine the thickness of fire brick and insulation which gives minimum heat loss. | CO2 | L4 | 6M |

**OR**

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|---|---|---|-----|----|----|
| 4 | a | What is lumped system analysis? Derive the expression for it  | CO2 | L3 | 6M |
|   | b | A 50 cm x 50 cm copper slab 6.25 mm thick has a uniform temperature of 300 °C. Its temperature is suddenly lowered to 36 °C. Calculate the time required for the plate to reach the temperature of 108. Take $\rho = 9000 \text{ kg/m}^3$ , $c = 0.38 \text{ kJ/kg } ^\circ\text{C}$ , $k = 370 \text{ W/m } ^\circ\text{C}$ and $h = 90 \text{ W/m}^2 \text{ } ^\circ\text{C}$ . | CO2 | L4 | 6M |

**UNIT-III**

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|---|---|--|-----|----|----|
| 5 | a | What is the physical significance of the Nusselt number? How is it defined.  | CO3 | L3 | 6M |
|   | b | Assuming that a man can be represented by a cylinder 350 mm in diameter and 1.65 m high with a surface temperature of 28 °C. Calculate the heat he would lose while standing in a 30 km/h wind at 12 °C. | CO3 | L4 | 6M |

**OR**

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|---|---|---|-----|----|----|
| 6 | a | Differentiate between laminar and Turbulent flow.   | CO3 | L3 | 6M |
|   | b | A horizontal plate measuring 1.5 m x 1.1 m and at 215 °C, taking upward is placed in still air at 25 °C. Calculate the heat loss by natural convection. The convective film coefficient for free convection is given by the following empirical relation $h = 3.05(T_f)^{1/4} \text{ W/m}^2 \text{ } ^\circ\text{C}$ . where $T_f$ is the mean film temperature in degree Kelvin. | CO3 | L4 | 6M |

**UNIT-IV**

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|---|---|--|-----|----|----|
| 7 | a | What are the applications of boiling and condensation process? | CO4 | L1 | 6M |
|   | b | Explain Stefan Boltzmann Law, Kirchhoff's Law.                 | CO4 | L1 | 6M |

**OR**

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|------------|---|------------|-----------|-----------|
| <b>8 a</b> | Distinguish between Boiling and Condensation.       | <b>CO4</b> | <b>L1</b> | <b>6M</b> |
| <b>b</b>   | What is black body? How is differ from a gray body? | <b>CO4</b> | <b>L1</b> | <b>6M</b> |

**UNIT-V**

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|----------|---|------------|-----------|------------|
| <b>9</b> | Derive the expression for Logarithmic Mean Temperature Difference (LMTD) in case of counter flow. | <b>CO5</b> | <b>L3</b> | <b>12M</b> |
|----------|---|------------|-----------|------------|

**OR**

- |           |   |            |           |            |
|-----------|---|------------|-----------|------------|
| <b>10</b> | In a certain double pipe heat exchanger hot water flow at a rate of 5000 kg/h and gas cooled from 95 °C to 65 °C. At the same time 50000 kg/h of cooling water at 30 °C enters the heat exchanger. The flow conditions are that L4overall heat transfer coefficient remains constant at 2270 W/m <sup>2</sup> K. Determine the heat transfer area required and the effectiveness, assuming two streams are in parallel flow. Assume for the both the streams $c_p = 4.2$ kJ/kg K. | <b>CO5</b> | <b>L4</b> | <b>12M</b> |
|-----------|---|------------|-----------|------------|

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